A Green Synthesis of 2-Ethylanthraquinone by Dehydration of 2-(4'-ethylbenzoyl) benzoic Acid over Solid Acid Catalysts

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Abstract: The dehydration of 2-(4'-ethylbenzoyl) benzoic acid (BE acid) to 2-ethylanthraquinone (2-EAQ) was investigated over solid acid catalysts. The results showed that H-beta zeolite catalyst modified by dilute HNO₃ solution exhibited an excellent performance. In our study, the conversion of BE acid can reach 96.7%, and the selectivity to 2-EAQ is up to 99.6%.

Keywords: 2-Ethylanthraquinone, 2-(4'-ethylbenzoyl) benzoic acid, H-beta, dehydration.

2-EAQ is an important intermediate for the synthesis of hydrogen peroxide, pharmaceuticals, pesticides, and dyes. With the increasing demand for hydrogen peroxide, it needs to enhance the yields of 2-EAQ. However, in the conventional process, concentrated H₂SO₄¹⁻² is employed as the catalyst in the dehydration of BE acid for the synthesis of 2-EAQ, which produces a series of environmental impacts and safety concerns. For these reasons, a substitute process, which has little or no hazards to environments, should be pursued. Recently, due to the special pore structure ³⁻⁴ and relatively high density of acid sites⁵, H-beta zeolite has attracted much attention in the synthesis of anthraquinone⁶⁻⁷. However, in the dehydration of BE acid into 2-EAQ, some undesired by-products, such as methylanthraquinon and anthraquinone, may be formed over H-beta zeolite catalyst, which leads to a lower selectivity to 2-EAQ. In this paper, we first reported the dehydration of BE acid for the synthesis of 2-EAQ over H-beta zeolite catalyst and a high selectivity to 2-EAQ was achieved through adjusting the acidity of the H-beta zeolite catalyst and the reaction conditions.

Experimental

The H-Y catalyst was prepared by calcining NH₄-Y (obtained from the Chinese Danyang Group) at 823 K for 4 h. The H-ZSM-5 zeolite and the H-Beta zeolite (SiO₂/Al₂O₃ = 22) were acquired by treating the sodium form zeolites (offered by the Institute of Industrial Catalysis, Dalian University of Technology). The obtained catalyst was calcined at 823 K for 4 h.

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The H-beta zeolite (SiO₂/Al₂O₃ = 22) was dealuminated by dilute HNO₃ solution with different acid concentration, and then we got the H-beta zeolites (SiO₂/Al₂O₃ = 107 and SiO₂/Al₂O₃ = 162). The obtained catalysts were calcined at 823 K for 4 h. From XRD (Rigaku D/max-2400) pattern, we observed that the crystal structure was not destroyed, when H-beta zeolite (22) was dealuminated by HNO₃ solution. The bulk SiO₂/Al₂O₃ ratio of the H-beta zeolite was determined by XRF (SRS-3400 X).

The reaction of BE acid dehydration was carried out in a batch reactor. In a typical experiment, the solid BE acid was first heated to the reaction temperature in the reactor, and then the catalyst was put into the reactor with continuous magnetic stirring. After a period of reaction, the reaction system was cooled, and the reaction mixture was treated with 1,4-diethylene dioxide, dissolving both product and reactant, followed by a separation in a centrifuge. The products were analyzed by liquid-chromatogram (Agilent 1100), using ZORBAX SB-C18 (250×4.6 mm) column at room temperature.

Results and Discussion

Table 1 shows the results obtained in the dehydration of BE acid on various zeolite catalysts under the studied reaction conditions, and H-beta exhibited an excellent performance. While both HY zeolite and H-ZSM-5 zeolite exhibited the low conversion of BE acid and low selectivity to 2-EAQ. It can be seen that over HY and H-ZSM-5 catalysts, most of BE acid was converted into MAQ. **Table 1** also shows the effect of SiO₂/Al₂O₃ ratio of H-beta zeolite on the reaction properties. The H-beta (107) exhibited the most excellent performance in the dehydration of BE acid, the conversion of BE acid reaches 85.9% and the selectivity to 2-EAQ is 95.9%. NH₃-TPD (CHEMBET-3000) and FTIR spectra of adsorbed pyridine (EXUINOX 55) revealed the changes of the acidity of H-beta with the changes of SiO₂/Al₂O₃ ratio. It can be concluded that the suitable acid nature and the suitable distribution of acid sites favored the dehydration of BE acid for the synthesis of 2-EAQ.

From **Table 2**, it can be seen that reaction temperature has a great effect on the conversion of BE acid and a slight effect on the selectivity to 2-EAQ. With the increasing of the reaction temperature, the conversion of BE acid increases dramatically, while the selectivity to 2-EAQ increases slowly. The conversion of BE acid reaches 96.7%, and the selectivity to 2-EAQ is up to 99.6% at 550 K.

Catalyst	conversion(%)	Production distribution (%)			Yield of 2-EAQ
		AQ	MAQ	2-EAQ	(%)
HY	3.5	1.9	73.6	18.4	0.6
H-ZSM-5	16.1	5.7	76.3	5.6	0.9
H-beta (22)	62.8	0.4	5.4	93.1	58.5
H-beta (107)	85.9	0.5	2.5	95.9	82.4
H-beta (162)	77.4	0.8	3.9	93.8	72.6

 Table 1
 The dehydration of BE acid over different catalysts

Notes: BE acid/catalyst =3.5 (g/g), Reaction temperature = 523 K, Reaction time= 1.5 h,

AQ= anthraquinone, MAQ=2-methylanthraquinone and 1-methylanthraquinone,

2-EAQ= 2-ethylanthraquinone

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Temperature (K)	conversion(%)	Produ	action distribu	Yield of 2-EAQ	
	-	AQ	MAQ	2-EAQ	(%)
523	62.8	0.4	5.4	93.1	58.5
540	92.0	0.1	2.4	97.4	89.6
550	96.7	0.4	0.0	99.6	96.3

 Table 2
 Effect of temperature on the dehydration of BE acid over H-beta (22)

Notes: BE acid/catalyst =3.5 (g/g) Reaction time= 1.5 h

Conclusion

H-beta zeolite catalyst is an efficient catalyst for the substitute of concentrate H_2SO_4 catalyst in the dehydration of BE acid for the synthesis of 2-EAQ. High selectivity to 2-EAQ can be achieved by adjusting the acidity of the H-beta zeolite catalyst and the reaction temperature.

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